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Simulation and testing of a latent heat thermal energy storage unit with metallic phase change materials

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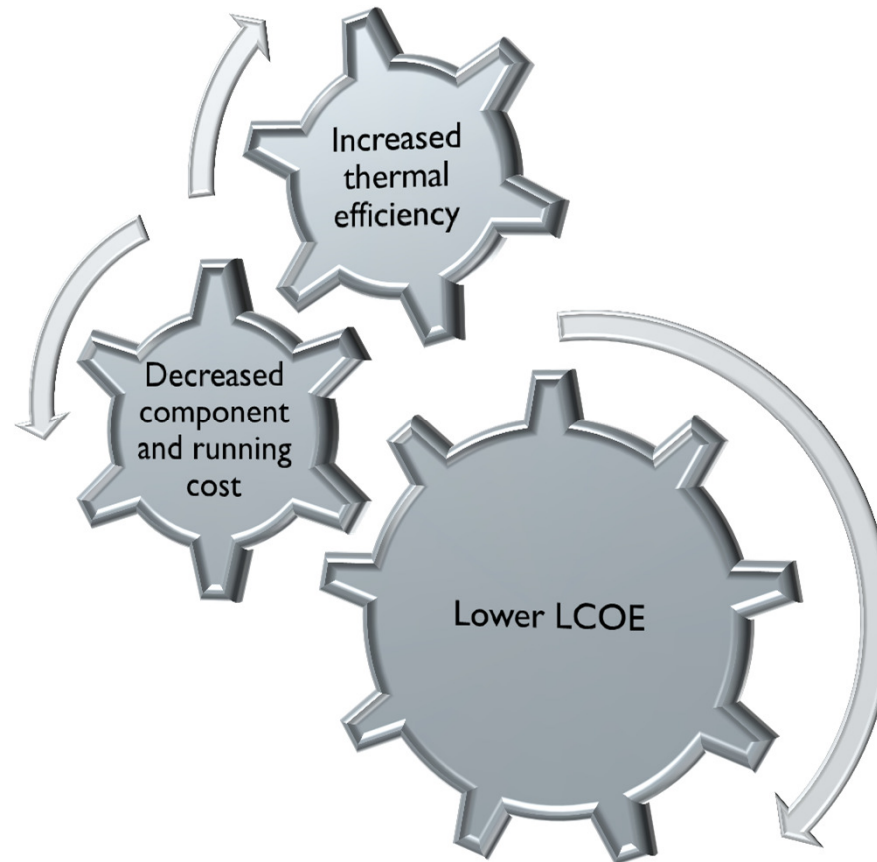
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Aims in CSP





Cost breakdown of a CSP plant (DOE case study)



Cost breakdown of LCOE (All costs)		
Heliostat cost	22.1	%
Indirect costs	20.8	%
Operations and maintenance	12.1	%
Power plant cost	12.1	%
Receiver cost	10.1	%
Tax	8.1	%
Storage cost	7.4	%
Balance of plant cost	4.0	%
Site cost	2.0	%
Tower cost	1.3	%

DOE – CSP calculation at 15 US\$ cents/kWh

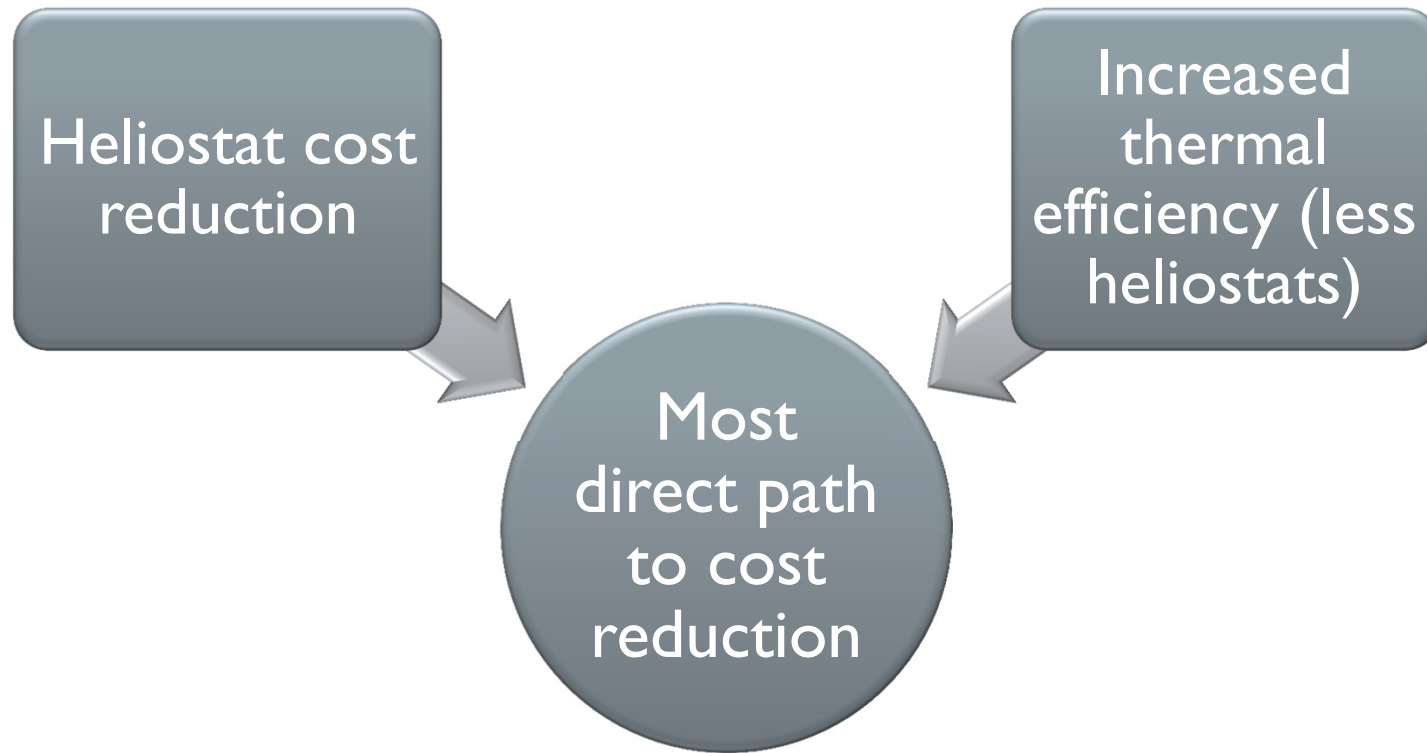
41% of the costs are due to indirect costs and is site specific

Still, heliostats relates to 37.5% of the total hardware cost



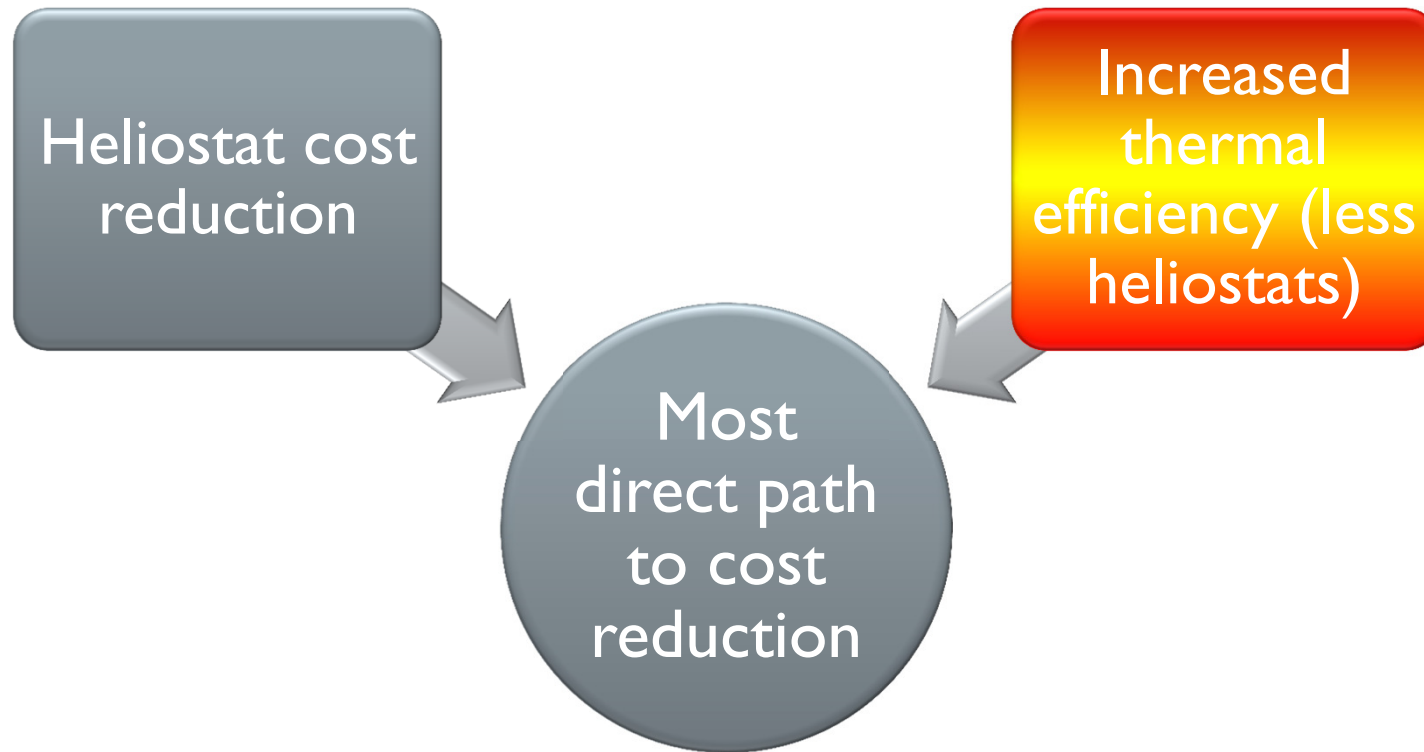


Most efficient method of cost reduction





Most efficient method of cost reduction





Increased thermal efficiency of power block



Technology	Source temperature	Thermal efficiency
Subcritical steam	540°C	~36%-40%
Supercritical / Ultra supercritical steam	600°C	~48%-52%
CO ₂ Brayton cycles (S-CO ₂)	550°C	~45%

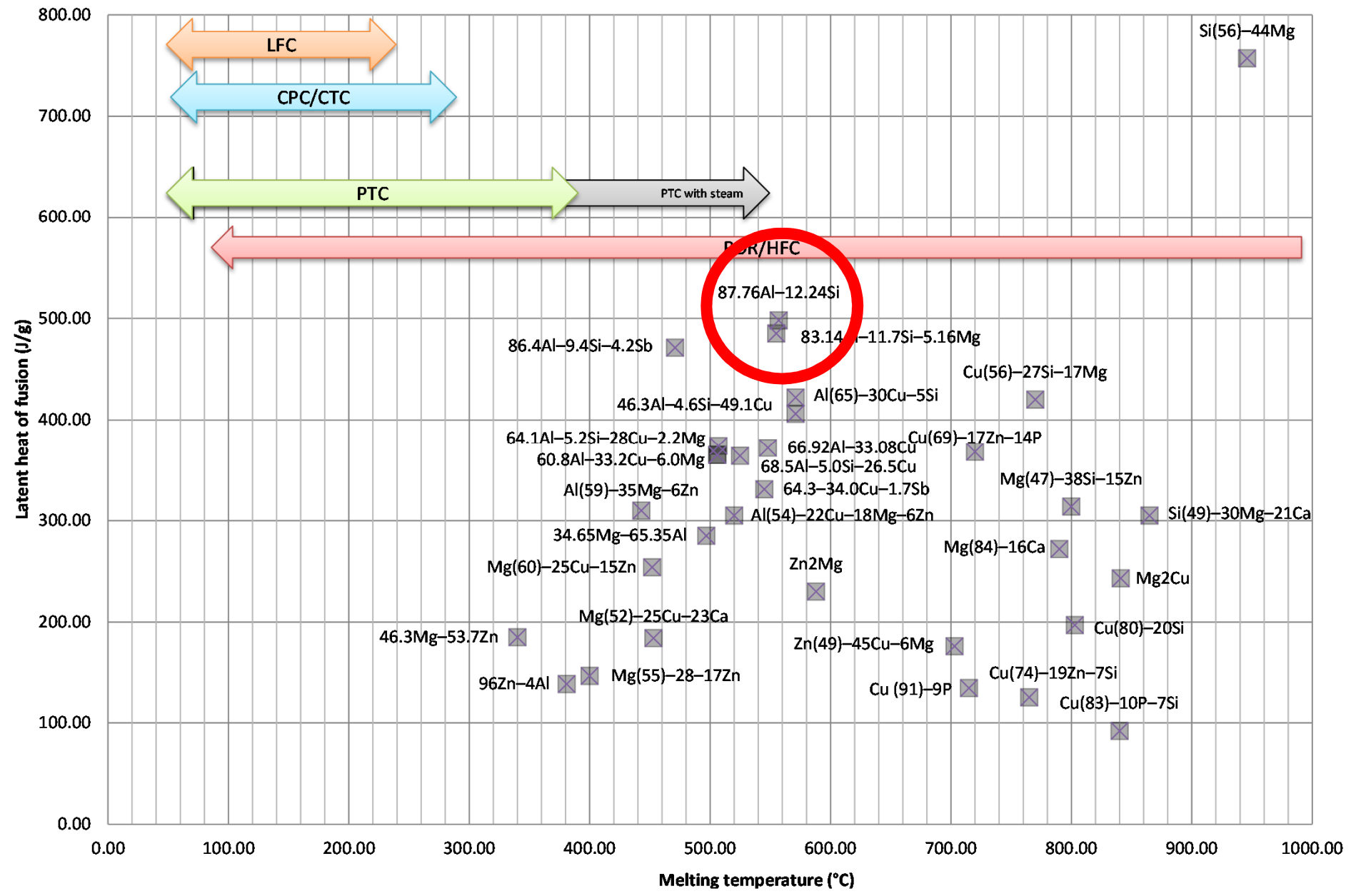
Higher source temperatures are required.

- Consider a 10% increase in thermal efficiency from a usual subcritical steam power block to a ultra supercritical steam power block:
 - 26.3% savings in thermal input from the heliostats.
 - 26.3% less heliostats
 - And a **5.8% reduction in LCOE**, and a 9.8% reduction in plant cost based on heliostats alone.





Metallic PCM – Material selection for research

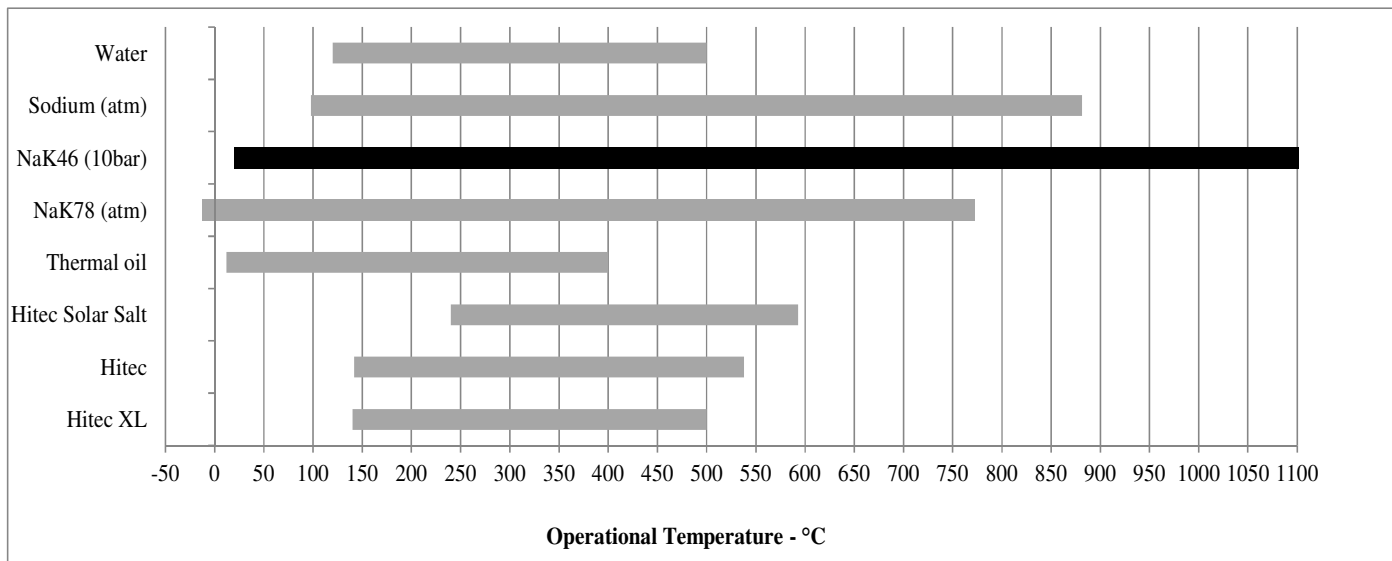




Heat transfer fluids

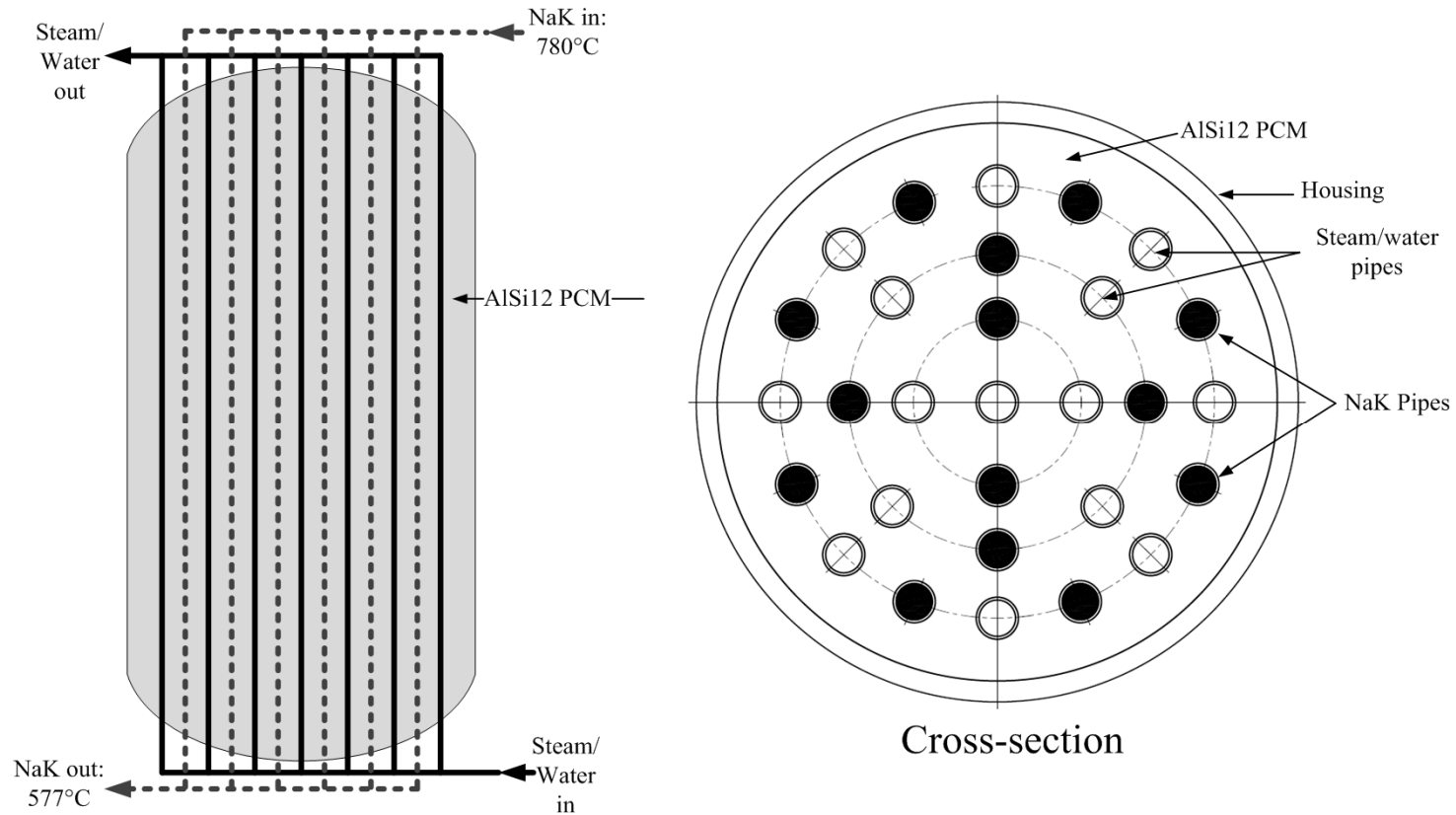


- Of all the HTFs, NaK is best suited for attaining higher receiver temperatures
- The low melting point means increased plant reliability, and lower operational cost.



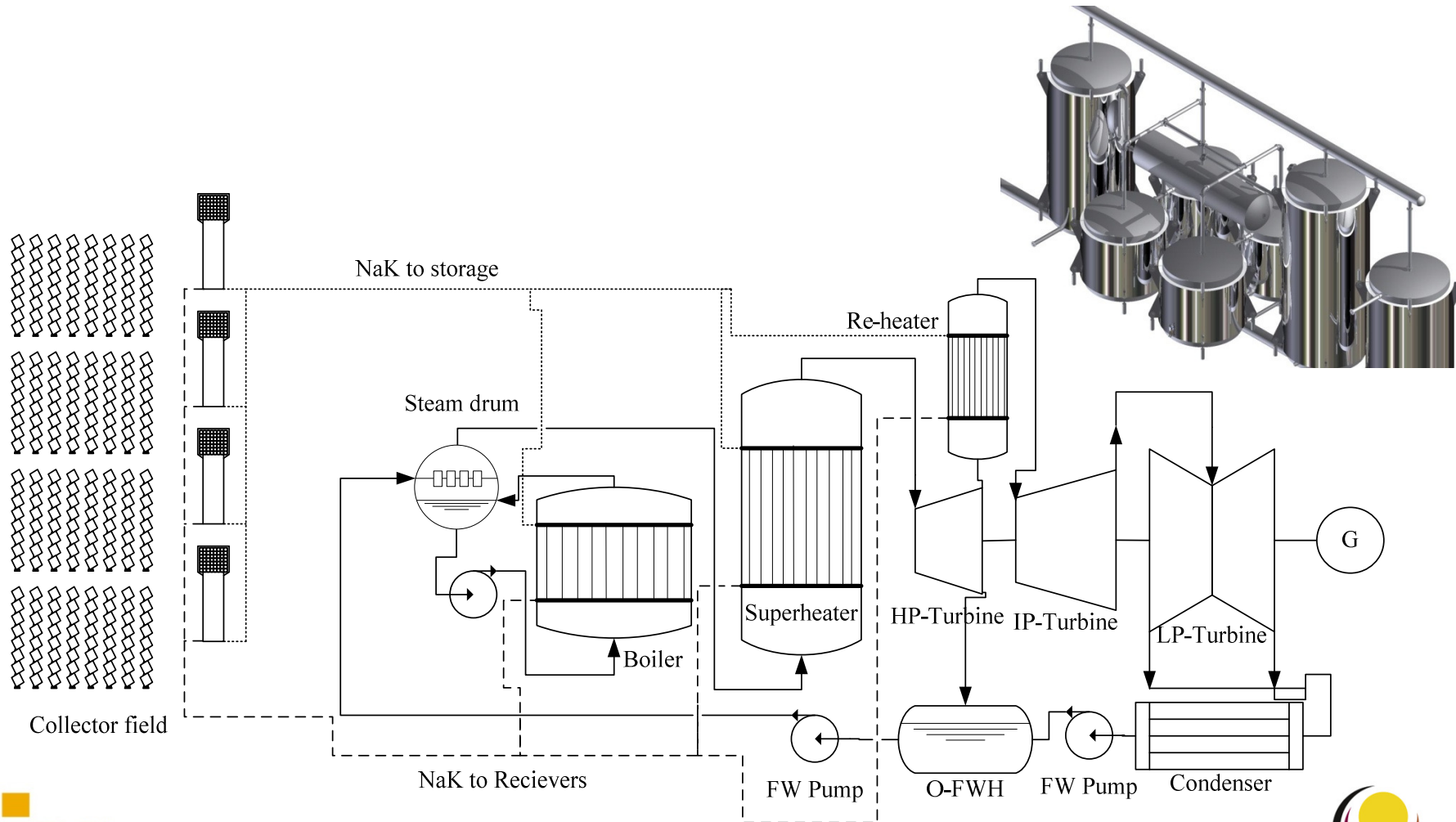


Introduction – Combined storage and steam generator concept



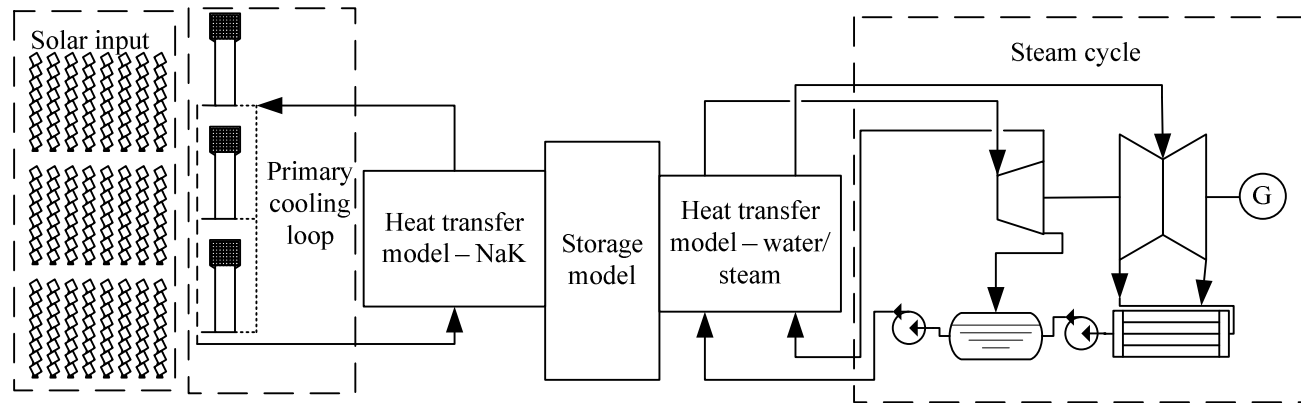


Potential concepts: Metallic phase change material – Direct steam generation from storage



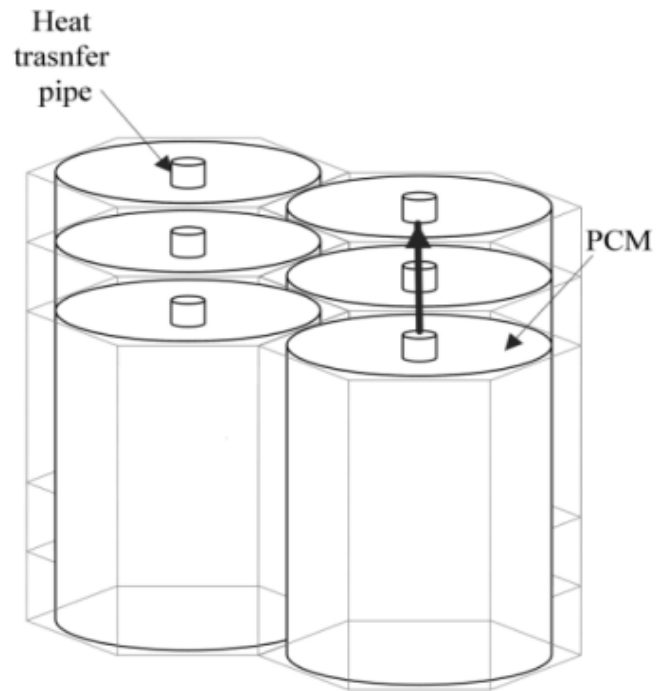


Simulation - Overview



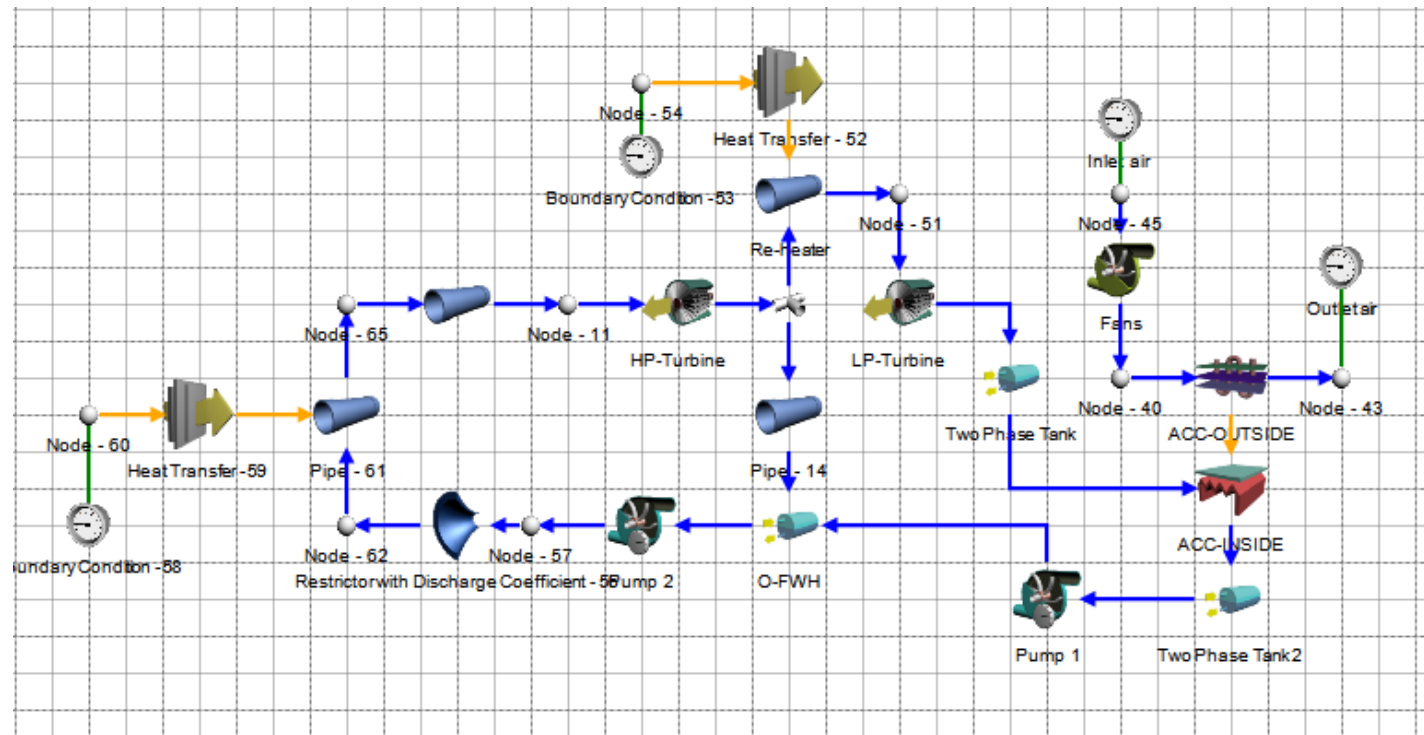


Discretization of heat storage unit





Simulation - Flownex

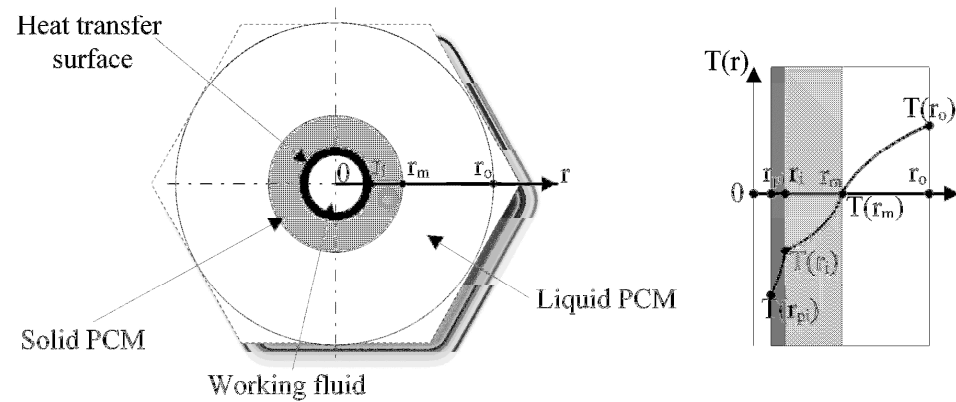




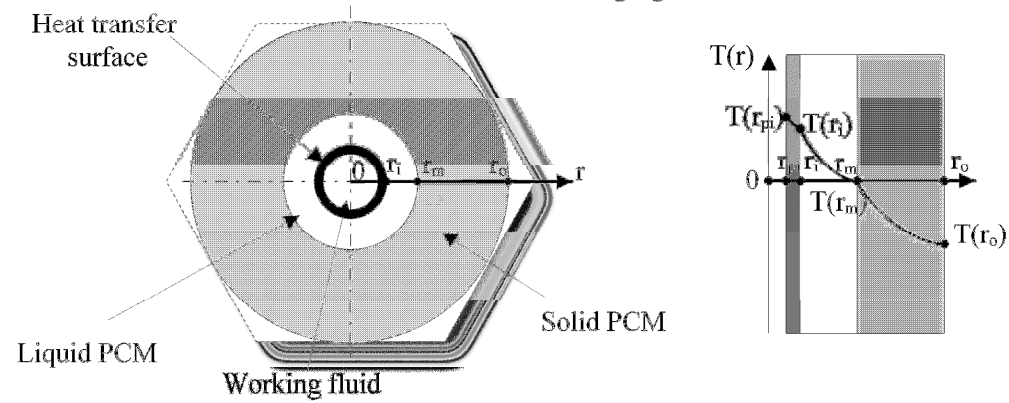
Transient state thermal model



Discharging



Charging





Mathematical formulation



Governing equation: One dimensional heat conduction equation

$$\frac{\delta T}{\delta t} = \alpha \frac{\delta^2 T}{\delta r^2} + \frac{\alpha}{r} \frac{\delta T}{\delta r}$$

Boundary conditions:

$$-kA \frac{\partial T(r_{pi}, t)}{\partial r} = Q_{oil}(t)$$

$$-k_p \frac{\partial T_p(r_i, t)}{\partial r} = k_{PCM} \frac{\partial T_{PCM}(r_i, t)}{\partial r} \quad T_p(r_i) = T_{PCM}(r_i)$$

$$\frac{dr_m(t)}{dt} = \frac{k_s}{\rho H_f} \frac{\partial T_s(r_m(t), t)}{\partial r} - \frac{k_l}{\rho H_f} \frac{\partial T_l(r_m(t), t)}{\partial r} \quad T_l(r_m) = T_s(r_m)$$



$$-k_p \frac{\partial T_p(r_o, t)}{\partial r} = 0$$





Implementation – Finite difference method



$$\frac{\delta T}{\delta t} = \alpha \frac{\delta^2 T}{\delta r^2} + \frac{\alpha}{r} \frac{\delta T}{\delta r}$$

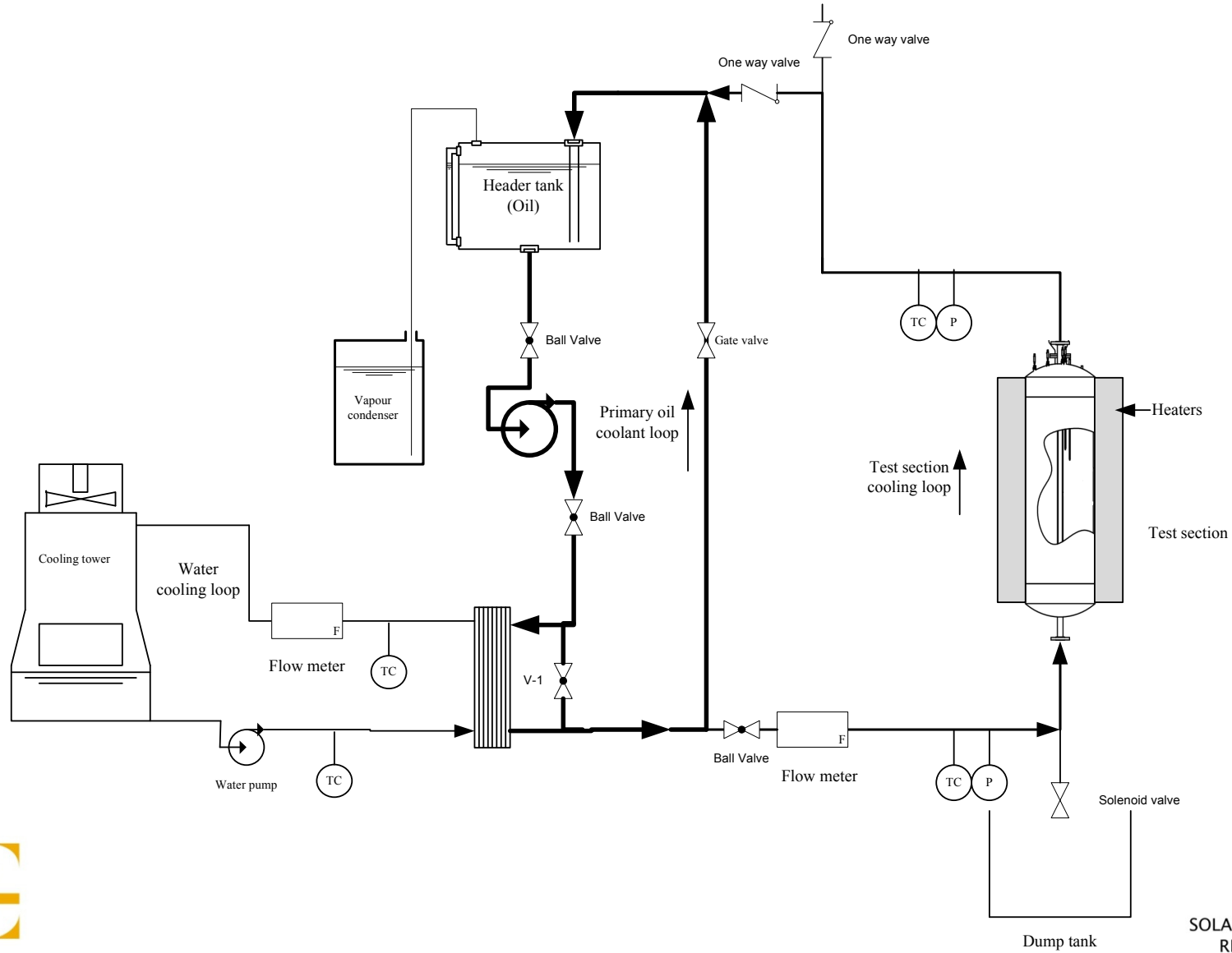
$$\frac{T_m^{p+1} - T_m^p}{\Delta t} = \alpha \frac{T_{m+1}^p + T_{m-1}^p - 2T_m^p}{\Delta r^2} + \frac{\alpha}{r} \frac{T_{m+1}^p - T_{m-1}^p}{2\Delta r}$$

- Boundary conditions had been implemented accordingly
- Moving boundary implemented through a energy balance



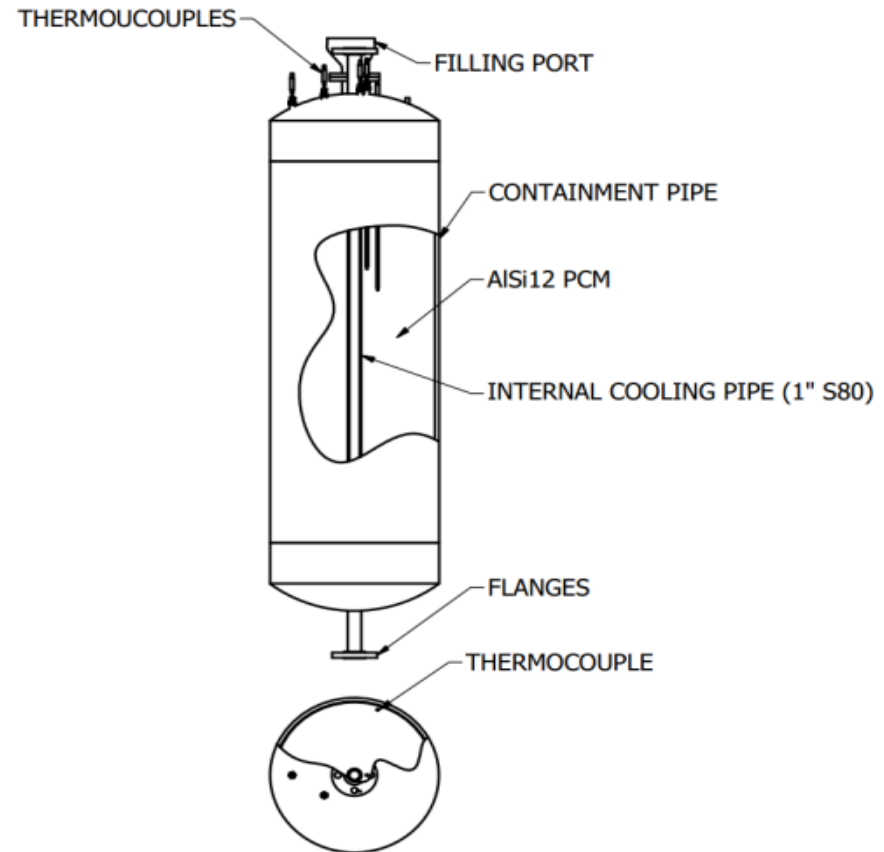


Experiment:





Cylinder geometry		
Outer cylinder		
Inside diameter	398	mm
Outside diameter	408	mm
Heat transfer pipe		
Inside diameter	24.4	mm
Outside diameter	33	mm
Length in contact with AISi12	1270	mm
Volume of AISi12	0.1533	m ³
Mass of AISi12	408	kg
Thermocouple placement from the centre		
Probe 1	30	mm
Probe 2	45	mm
Probe 3	90	mm
Probe 4	135	mm
Probe 5	180	mm





Experiment:



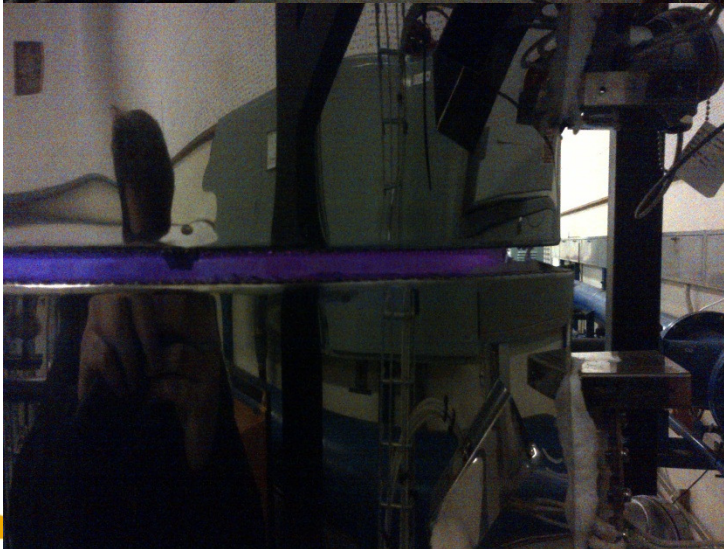
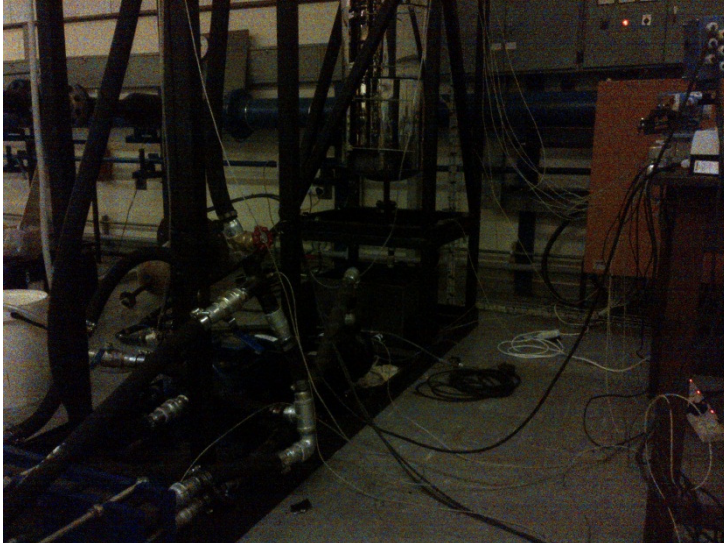


Experiment:





Experiment:



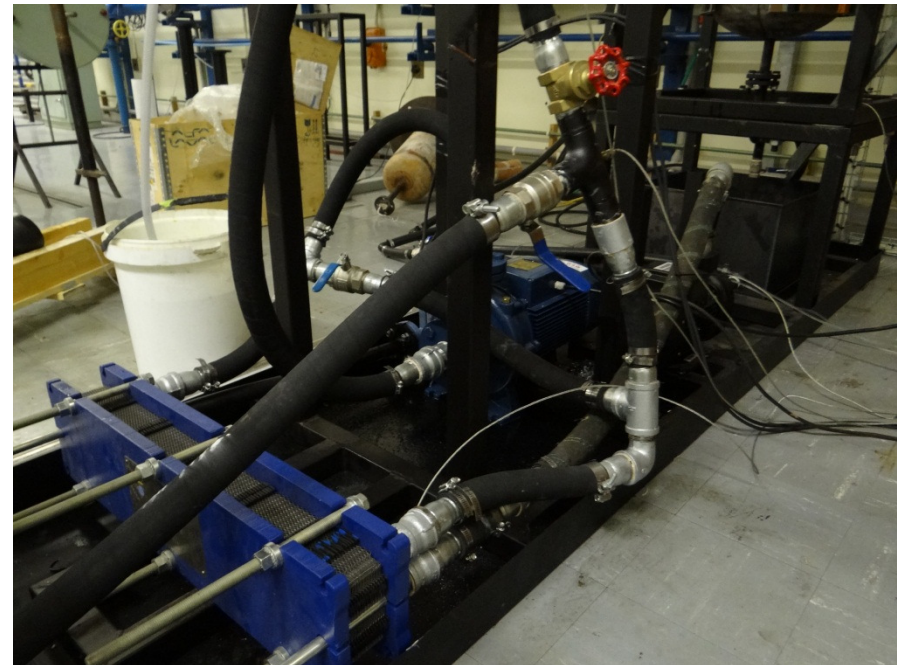


Experiment:



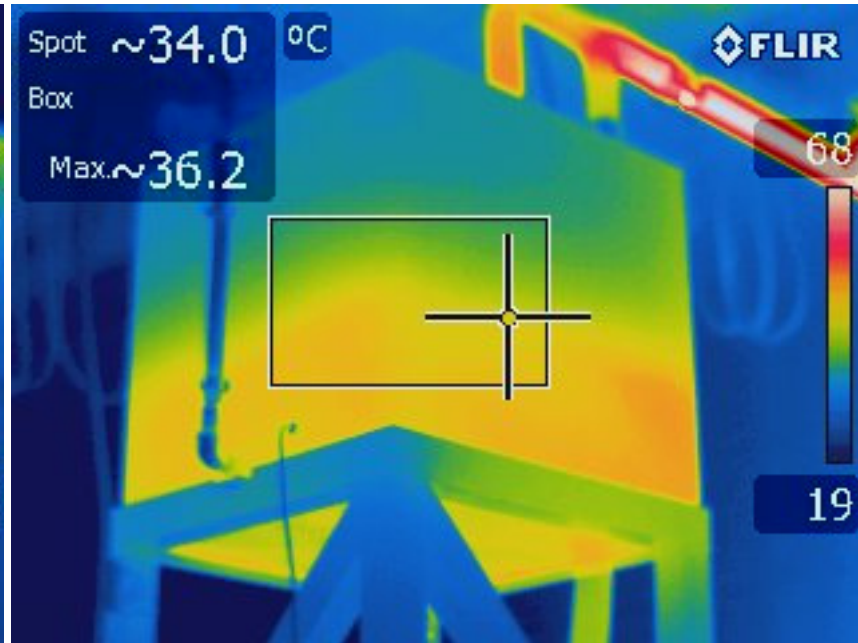
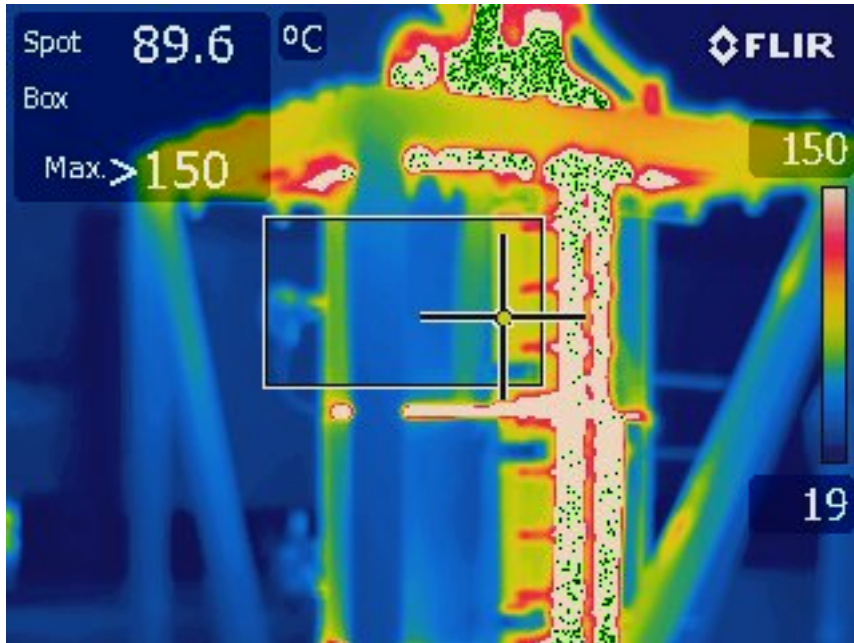


Experiment:





Experiment:





Thermal properties:

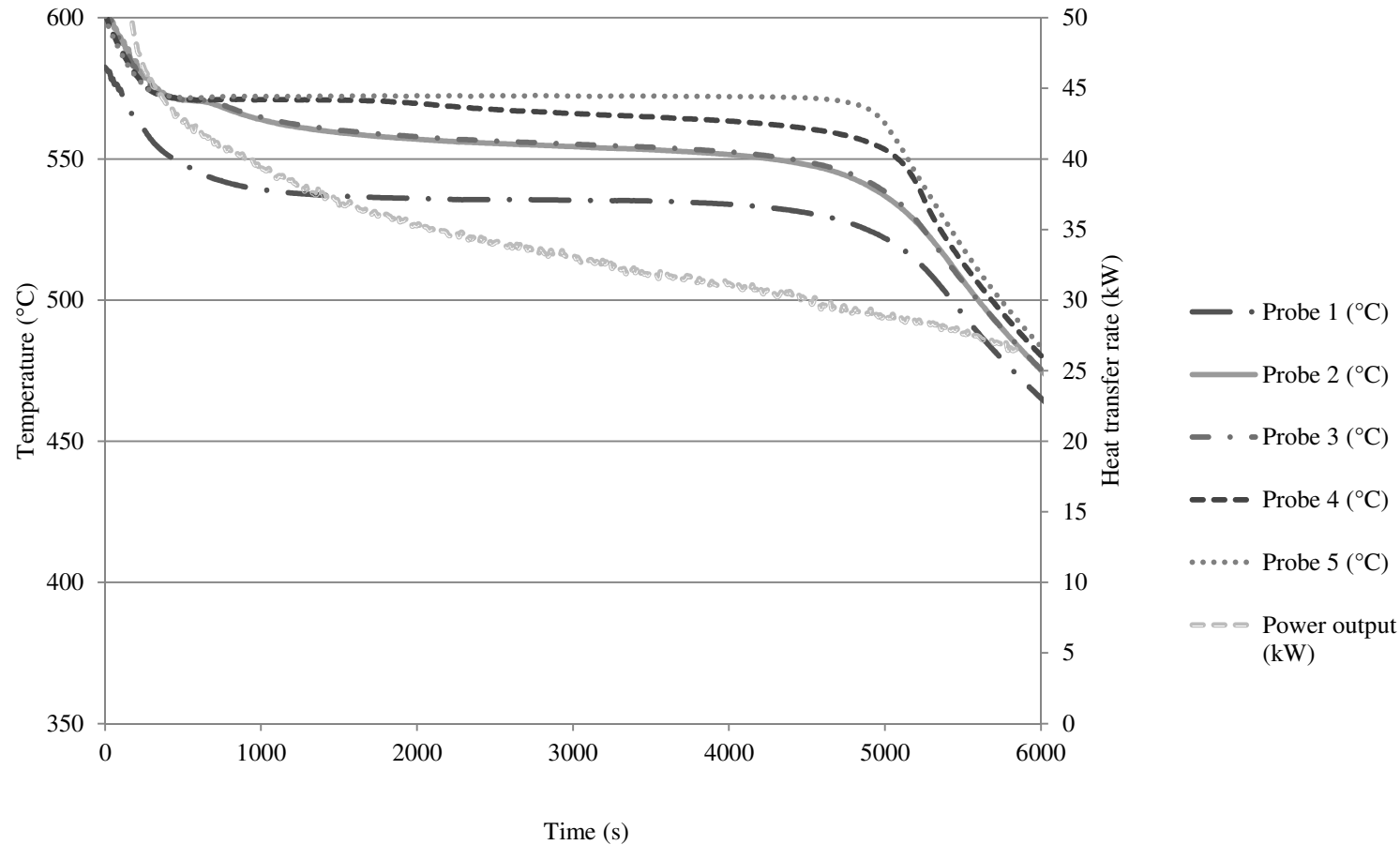


Thermophysical properties of AISi 12			Source
Density	2661	kg/m ³	[5]
Specific heat	0.939	kJ/kg.k	[5]
Heat of fusion	515	kJ/kg	[5] / Measured: DSC
Phase change temperature	577	°C	[5] / Measured: DSC
Thermal conductivity	181	W/m.K	[5]
Thermophysical properties of Mild steel			
Density	7854	kg/m ³	
Specific heat	1.169	kJ/kg.k	
Thermal conductivity	30	W/m.K	
ISO 100 quenching oil			
Density at 60 °C	890	kg/m ³	Measured: Lab
Specific heat at 60 °C	1.950	kJ/kg.K	Measured: MDSC
Kinematic viscosity at 60 °C	20.2	mm ² /s	Measured: ASME I 32 I





Experimental results:

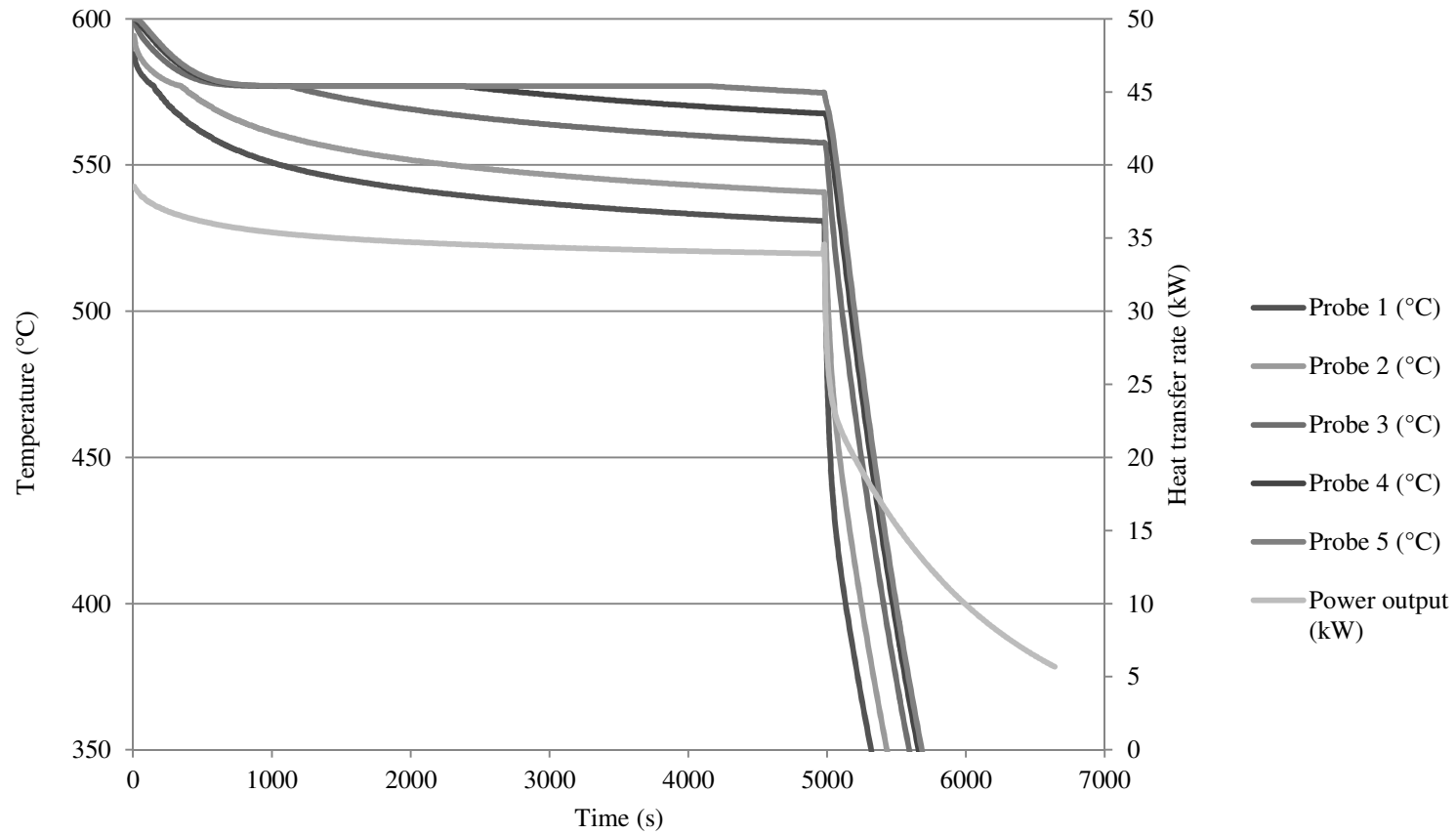


- 78.5 minutes of isothermal discharge at a average of 35kW
- 577°C
- It is clear that the movement of the solidification front do not influence



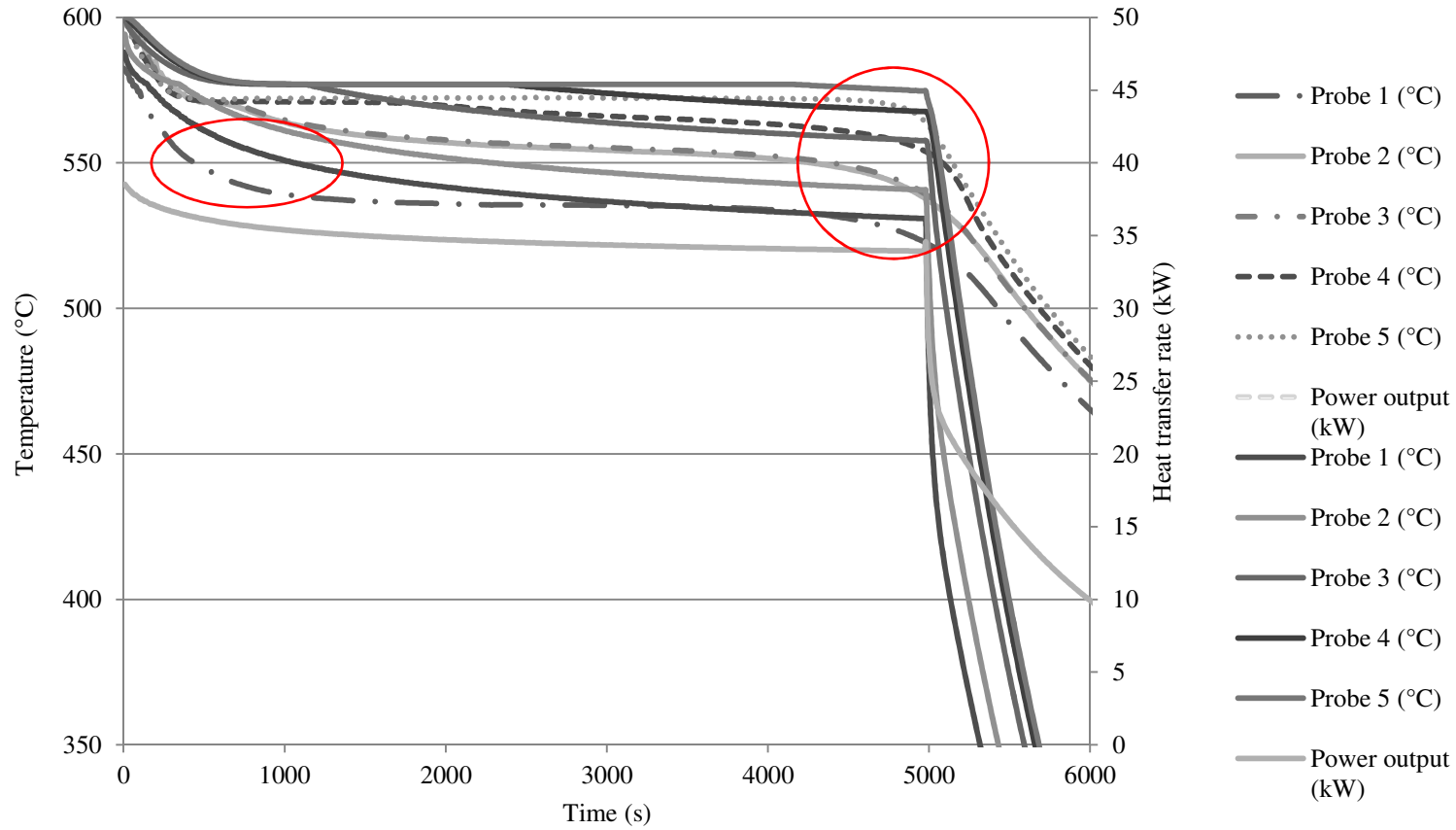


Experimental results:





Experimental results:





Conclusions

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- A prototype latent heat thermal energy storage unit has been built and tested.
- Isothermal storage has been achieved
- It is possible to predict the latent heat discharge process, but more work is needed on the sensible cooling model. This will increase the accuracy of the overall model.



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Acknowledgments



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